## Johnstown Water Treatment Plant Expansion

Comparison of Project Costs Between Membrane Filtration/Granular Activated Carbon & Ozone/Biologically Active Filtration

June 4, 2021

Three project fees were included with Burns & McDonnell's proposal of February 5, 2021. Town staff indicated their preference for Option 3, which is a comprehensive site plan based on Membrane Filtration and Granular Activated Carbon (GAC). Subsequent discussions with the Town, as well as a working session with the Town Council on April 12, 2021, lead the project team toward Ozone and Biologically Active Filtration (BAF) as the preferred solution for addressing growing demand, aging infrastructure and on-going taste and odor issues (Option 4).

Option 4 will provide robust treatment for current and future water quality issues and regulations, as well as *effective treatment of high taste and odor issues* related to cyanobacteria in the Town's water supply. However, Ozone/BAF will increase the amount of equipment and complexity of upgrades to the Johnstown WTP. This will increase the construction cost, as well as the related engineering effort. Colorado Department of Public Health and Environment (CDPHE) Water Quality Control Division will require piloting of both Ozone and BAF before approval.

Table 1 compares the anticipated taste and odor removals, construction cost, operating costs and schedules of Option 3 (Membrane Filtration/GAC) and Option 4 (Ozone/BAF). Options 1 and 2 are not discussed because they do not meet all project objectives identified during the Town Council working session of April 12, 2021, in particular, taste and odor control. Costs are based on two phases to build-out capacity, with Phase 1 at a capacity of 12.5 million gallons per day (MGD).

	Table 1: Comparison of Key Considerations													
Approach	Option 3	Option 4												
Process	Membrane Filtration/GAC	Ozone/BAF												
Summary														
Taste & Odor	60 to 80%	90 to 99%												
Removals														
Annual O&M	\$391,000	\$69,000												
Costs <sup>1</sup>														
Capital Costs	\$20M to \$35M	\$45M to \$60M												
Implementation	30 months	37 months												
Timeline														

1. O&M cost for taste and odor removal only to compare GAC to Ozone generation. Includes electricity, chemical and carbon replacement costs only.

### Membrane Filtration/GAC (Option 3) offers:

- Less removal of taste and odor compounds.
- Lower construction cost, due to the simplified nature of the Membrane Building (slab on grade with pre-engineered metal building).
- Higher taste and odor operating costs due to change-outs of the activated carbon multiple times per year.
- Easily scalable for future phases.
- Maintains the use of the existing granular media filters in the short term.
- Relies on existing infrastructure (filter building, storage tanks).
- Integrates the 6 GAC vessels purchased in 2021 into the WTP expansion.

### Ozone/BAF (Option 4) offers:

- High removals of up to 99% taste and odor compounds.
- Higher construction cost, due to the complex buildings required for ozone system, ozone contact basin, new deep bed filters and new chemical systems.
- Lower taste and odor operating costs for electricity, oxygen and biological filtration chemicals compared to the carbon changeout costs.
- More expensive expansion at the next phase.
- Does not rely on aging infrastructure. Existing filters are abandoned.
- Positions the Town for changes in raw water quality (wildfire, drought, nutrient run off) and future treatment regulations.
- Requires 8-week piloting of ozone and BAF.

Both options will provide effective removal of taste and odor compounds. The GAC option will rely on upstream steps (PAC at Lonetree, ultrasonic buoys at Town Lake, DAF optimization) in a multi-phased approach to extend the life of the activated carbon. Ozone/BAF will be effective on its own across a wide range of water quality. The 2021 demonstration project will prove the effectiveness of GAC, as well as provide data on how often the carbon will need to be changed (\$228,000 each re-bed, up to 2 per year).

# Even if Ozone/BAF is selected at the start of the design phase, the Town will have an option to switch to a Membrane Filtration/GAC solution if the data from this summer shows the GAC working well.



## Assumed Ozone/BAF Site Layout



Figure 1 - Ozone/BAF Site Layout



Figure 2 - 3D Model of Ozone/BAF Filter Building

Table 2: Project Cost Comparison at 12.5 MGD <sup>1</sup>													
Approach	Option 3	Option 4											
Process Summary	Membrane Filtration/GAC	Ozone/BAF											
Div 01 - General Requirements	\$-	\$-											
Div 02 - Existing Conditions	\$236,000	\$298,000											
Div 03 - Concrete	\$1,866,000	\$5.840.000											
Div 04 - Masonry	\$342,000	\$691.000											
Div 05 - Metals	\$1.698.000	\$2,963,000											
Div 06 - Wood, Plastics and Composites	\$204,000	\$275,000											
Div 07 - Thermal and Moisture Protection	\$47,000	\$121,000											
Div 08 - Openings	\$148,000	\$213,000											
Div 09 - Finishes	\$181,000	\$287,000											
Div 10 - Specialties	\$17,000	\$30,000											
Div 11 – Equipment	\$17,000	\$20,000											
Div 12 - Furnishings	\$43,000	\$50,000											
Div 13 - Special Construction	\$17,000	\$40,000											
Div 14 - Conveying Equipment	\$51,000	\$160,000											
Div 21 - Fire Suppression	\$170,000	\$200,000											
Div 22 - Plumbing	\$255,000	\$450,000											
Div 23 - HVAC	\$679,000	\$1,200,000											
Div 26 - Electrical	\$1,527,000	\$3,400,000											
Div 27 - Communications	\$-	\$-											
Div 28 - Electronic Safety and Security	\$26,000	\$30,000											
Div 31 – Earthwork	\$1,301,000	\$3,465,000											
Div 32 - Exterior Improvements	\$179,000	\$250,000											
Div 33 - Water Utility	\$1,951,000	\$3,383,000											
Div 40 - Process Integration	\$-	\$-											
Div 41 - Conveying Systems	\$-	\$-											
Div 46 - Water Treatment Equipment	\$4,286,000	\$9,158,000											
SUBTOTAL	\$15,241,000	\$32,524,000											
General Requirements (12%)	\$1,829,000	\$3,903,000											
Construction Cost Sub-Total	\$17,070,000	\$36,427,000											
Contractor Overhead & Profit (15%)	\$2,561,000	\$5,465,000											
CONSTRUCTION COST	\$19,631,000	\$41,892,000											
Contingency (20%)	\$3,927,000	\$8,379,000											
Design Phase Engineering (6%)	\$1,178,000	\$2,514,000											
Construction Phase Engineering (6%)	\$1,178,000	\$2,514,000											
TOTAL PROJECT COST <sup>2</sup>	\$25,914,000	\$55,299,000											

#### CONFIDENTIDAL, NOT FOR EXTERNAL USE

- EOPCC in this study were completed in accordance with the Association for the Advancement of Cost Engineering (AACE) Class 5 definition. Class 5 EOPCC are generally developed with limited information (<5% defined) and subsequently vary in their accuracy. They are typically used for project screening, determination of feasibility, concept evaluation, and preliminary budget approval. The expected accuracy range is -20% to -50% below and +30 to +100% above. Vendor quotes were sought and gross unit costs/ratios from past projects were used to develop the estimates in this report. The EOPCC presented in this study are based on 2021 dollars at the time of issue. The use of the costs presented in this study should be escalated if used for future purposes to reflect changes in labor, material, and equipment. Local cost data or published cost indices should be consulted to determine an appropriate cost escalation factor.
- 2. Excludes land acquisition costs, permitting and legal fees.

Table 3: Engineering Comparison													
Approach	Option 3	Option 4											
Process Summary	Membrane	Ozone/BAF											
-	Filtration/GAC												
CONSTRUCTION COST	\$19,631,000	\$41,892,000											
Contingency (20%)	\$3,927,000	\$8,379,000											
SUBTOTAL CONSTRUCTION COST	\$19,631,000	\$41,892,000											
Engineering Task Series <sup>1</sup>													
100 - Project Initiation & Coordination	\$41,414	\$132,603											
200 - Review Existing Data & Basis of Design	\$177,297	\$607,074											
200A - Pilot Testing	NA	\$194,456											
300 - Preliminary Design 30%	\$177,560	\$402,333											
400 - Detailed Design 60%	\$189,499	\$444,163											
500 - Optimize Operations (Short Term Relief)	\$50,805	\$93,939											
600 - Final Design	\$165,556	\$374,778											
700 - Bid Phase Support <sup>2</sup>	\$11,891	\$11,891											
Design Phase Engineering <sup>3</sup>	\$814,022	\$2,261,237											
Estimated Owner Costs for Piloting <sup>4</sup>		\$180,000											

1. Engineering tasks based on a Design-Bid-Build project delivery model. Schedule and cost savings anticipated if the project is completed using a collaborative delivery model, such as Design-Build.

2. Bid Phase Support task series not required with a Design-Build delivery model. Engineering services for bidding and procurement integrated into Phase 2 Construction Services under a Design-Build delivery model.

3. Engineering services during design only. Construction phase engineering support negotiated near completion of design once construction complexity, delivery model, contractor and schedule are better defined.

4. Estimated owner costs for piloting include leasing of piloting equipment (Ozone and BAF trailers), temporary chemical systems, utilities, installation costs, operations and monitoring costs and laboratory analytical costs.

Table 4: Additional Design Effort for Option 4											
Approach	Option 3	Option 4									
Process Unit	Membrane Filtration/GAC	Ozone/BAF	Design Fee Adder	Additional Design Hours							
Lonetree Pump Station & Pipeline	Remain as	is	\$-	-							
Town Lake Pump Station	Remain as	is	\$-	-							
Raw Water Tank	Remain as	is	\$-	-							
Chemical Storage	Add Storage and Membrane Cleaning Systems to new Membrane Building	Add 4 new chemical systems for advanced oxidation and BAF (hydrogen peroxide, ammonium sulfate, sodium bisulfite, phosphoric acid). Relocate existing chemicals (coagulant, sodium hypochlorite, sodium hydroxide) to the new Filtration Building. Size chemical systems for ultimate capacity of 18 MGD.	\$175,000	950							
Pretreatment Capacity	Convert to SAF at 12.5	MGD capacity	\$-	-							
Filtration	Add Storage and Membrane Cleaning Systems to new Membrane Building. Includes two new systems for membrane cleaning (citric acid and sodium bisulfate) and relocation of two chemical systems (sodium hypochlorite and sodium hydroxide). Sized at capacity of 12.5 MGD. Membrane Building as slab on grade with pre-engineered metal superstructure	Add 4 new deep-bed filters (60-inch, 3.9 MGD each) to replace existing GMF. Includes settled water distribution channel, pipe gallery, new filter boxes with underdrains and backwash troughs, air scour system, and backwash waste collection. Biologically active for taste and odor control. Deep location determined by the hydraulic grade of existing pretreatment. New Filtered Water Tank below filter gallery, including a combination filtered water and backwash supply pump station. Complex concrete basins below grade. Pre-engineered metal superstructure.	\$225,000	1,200							
Taste & Odor Control	Implement multi-phase approach. Lease to own GAC contactors in Membrane Building. Optimize T&O removal with SAF conversion. Future flexibility for T&O control.	<ul> <li>Multi-phase approach. Improve PAC at Lonetree pump station, install ultrasonic buoys at Town Lake, optimize removals in SAF.</li> <li>Add <i>intermediate ozone</i> (after pretreatment), including liquid oxygen storage, vaporizers, injection skids, generators, concrete Ozone Contact Basin with serpentine baffles, ozone destructor units. Complex stainless steel piping, instrumentation, and controls. Assumed high levels of raw water bromide creating the need for hydrogen peroxide to mitigate bromate formation (disinfection by-product). Use of hydrogen peroxide will also minimize the volume of the Ozone Contact Basin.</li> </ul>	\$275,000	1,500							
Piloting	No piloting required.	CDPHE requirement for approval. Approximately 2 months of piloting required to determine ozone dose, capacity of ozone system, and BAF filter loading rate.	\$215,000	1,200							
Disinfection Compliance	Add new Disinfection Contact Basin (I	DCB) sized for ultimate flows.	\$-	-							
Treated Water Storage	Convert GST to distribution storage	Add 1,500,000 gallons of distribution storage in same tank as new DCB. Convert the GST to distribution storage.	\$75,000	400							
Distribution Pump Station	New at-grade pump station with vertical t	urbine pumps above a new DCB.	\$-	-							
Backwash Supply	Backwash from distribution system	Add Filtered Water Tank below filters. Need non-chlorinated backwash supply water for BAF (not able to take from storage tanks or distribution system). Add combination pump station with filtered water pumps to transfer water to the DCB and backwash supply pumps for the filters.	\$150,000	800							
Backwash Waste	No change	Existing backwash pond demolished to create space for the new Filter Building. Add new Backwash Waste Tank with combination pumps station. Recycle pumps to transfer supernatant to the front of the WTP. Backwash waste pumps to send waste to the existing sanitary sewer at a higher elevation than the Backwash Waste Tank.	\$150,000	800							
Electrical System	New electrical service for Membrane Building, DCB and DPS. Add second diesel generator. Upgrade site lighting and security	Similar to Option 3 but expanded for the additional process systems and equipment.	\$80,000	400							
SCADA System	Add control system nodes for Membrane Building, T&O system, DCB and new DPS.	Replace existing SCADA with new network for complex operations and new process units (Ozone, BAF, Filtered Water and Backwash Supply Pump Station, DCB, DPS, Recycle and Backwash Waste Pump Station).	\$60,000	300							

Approach	Option 3	Option 4		
Process Unit	Membrane Filtration / GAC	Ozone / BAF	Design Fee Adder	Additional Design Hours
Project Execution	As proposed.	Extended management and supervision for longer design schedule.	\$10,000	50
Additional Cost & Hours			\$1,415,000	7,600 hours
Summary	<b>Best Value Project, Limited T&amp;O Removals</b> Option 3 provides comprehensive site plant with future flexibility and operational robustness. Limited taste and odor removals with Membrane Filtration/GAC at higher operating costs.	<b>Robust &amp; Effective Operations for Water Quality Concerns</b> Address current and future T&O issues at higher certainty with fewer treatment steps, reduced operating costs when compared with Membrane Filtration /GAC, expanded WTP set up for future regulations and water quality events which may impact your watershed, phasing plan with flexibility to meet your budget.		

					2	021						2022												2023											2024			
ACTIVITY	MAR	APR	MAY	NOC	lic	AUG	SEP	ocr	NON	DEC	NAU	FEB	MAR	APR	MAY	NDC	il.	AUG	SEP	ocr	NON	DEC	NAU	FEB	MAR	AFR	MAY	NUC	ii,	AUG	SEP	ocr	NON	DEC	NAU	FEB	MAR	APR
OPTION 3 - MEMBRANE FILTRATION / GAC																																						
DESIGN																																						
BIDDING																																						
CONSTRUCTION																																						
OPTION 4 - OZONE / E	BAF																																					
DESIGN																																						
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Figure 1 - Schedule Comparison, assuming June 1 start