



Municipal Case Study

Biogas → RNG → Pipeline Injection

Tim Runde, Des Moines WRA

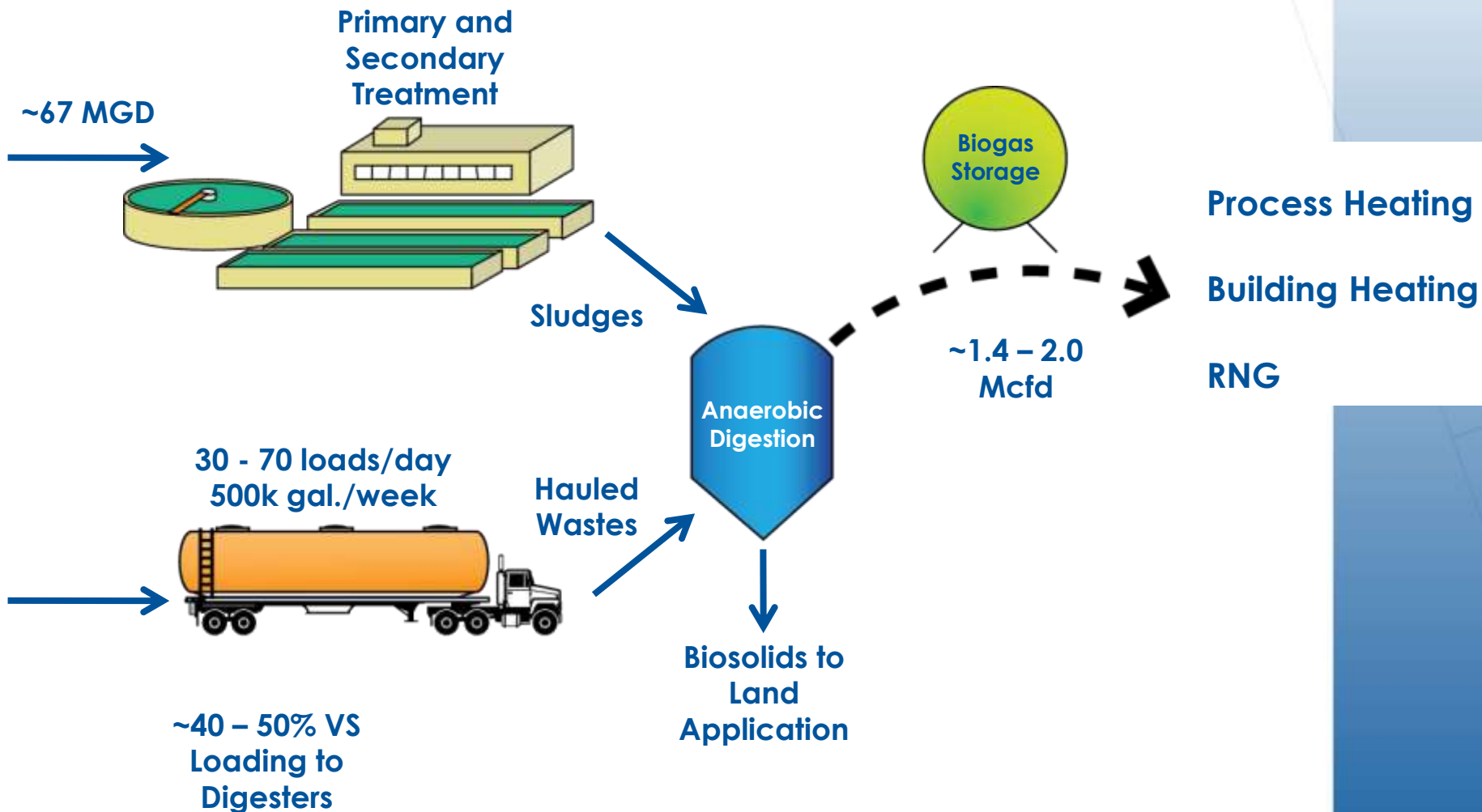


Des Moines Wastewater Reclamation Authority (WRA)



- WRA Serves 18 member agencies in three counties
- City of Des Moines is the contract operator of the WRA's wastewater reclamation facility (WRF)
- Average dry-weather flows of ~67 million gallons per day (MGD)
- Serves >600,000 residents in greater metro Des Moines area
- Completed \$20M Anaerobic Digestion Improvements Project in Spring 2014
- Completed \$19M Biogas Injection Project in October 2020

Des Moines WRF Flow Schematic:



Co-Digestion Waste Sources

- Restaurant Grease Trap / Interceptor Waste
- Dairy Waste
- Biodiesel Waste
- Slaughterhouse / Meat Processing Waste
- Lutein / Protein Waste
- Waste Soy Oil
- Sewage Sludge
- Sugar Waste
- Rendering / Gelatin Waste
- Corn Syrup / Mash



Evolution of Hauled Waste Receiving



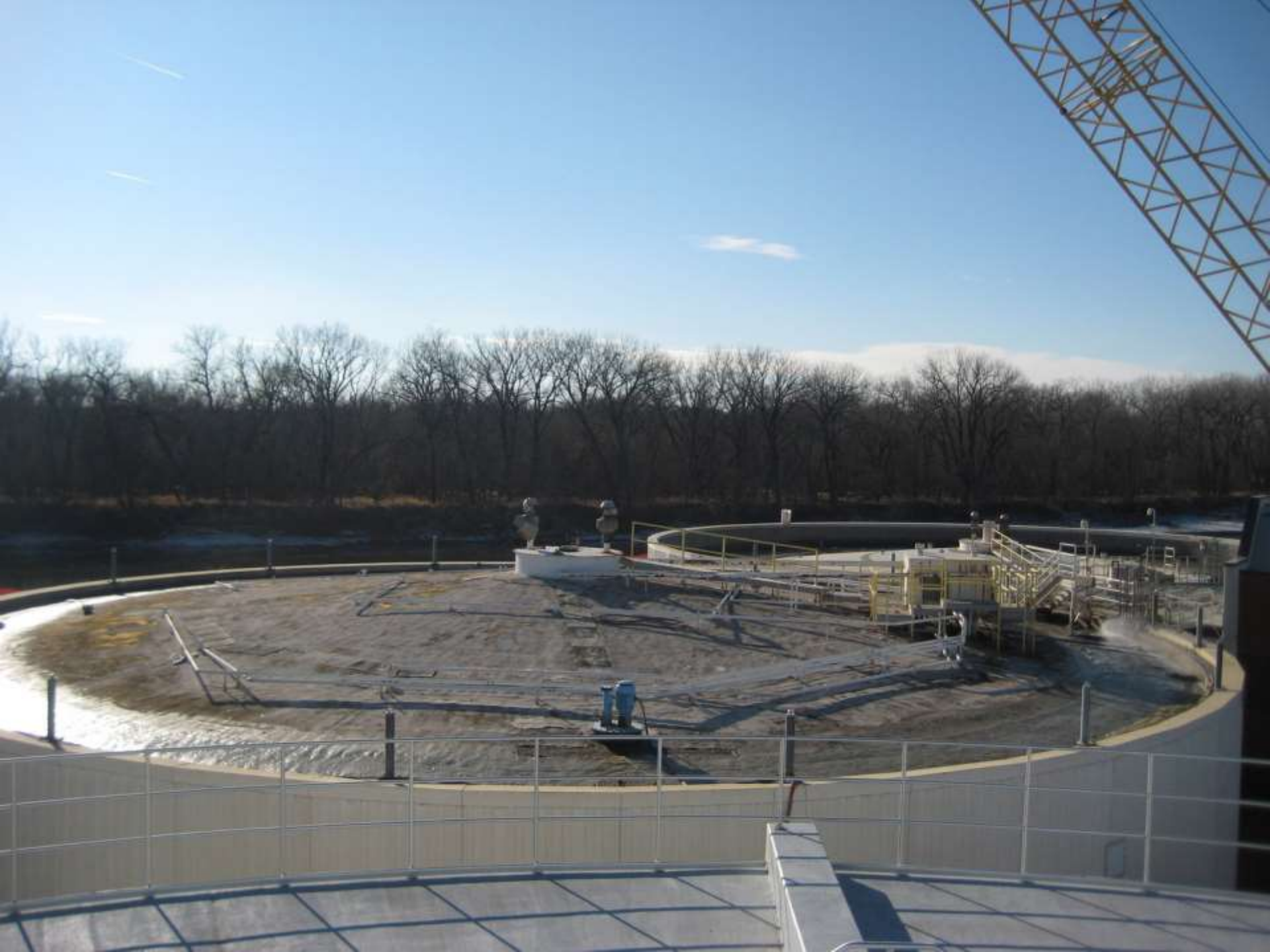
Simple pipe offloading
~1994 - 2006

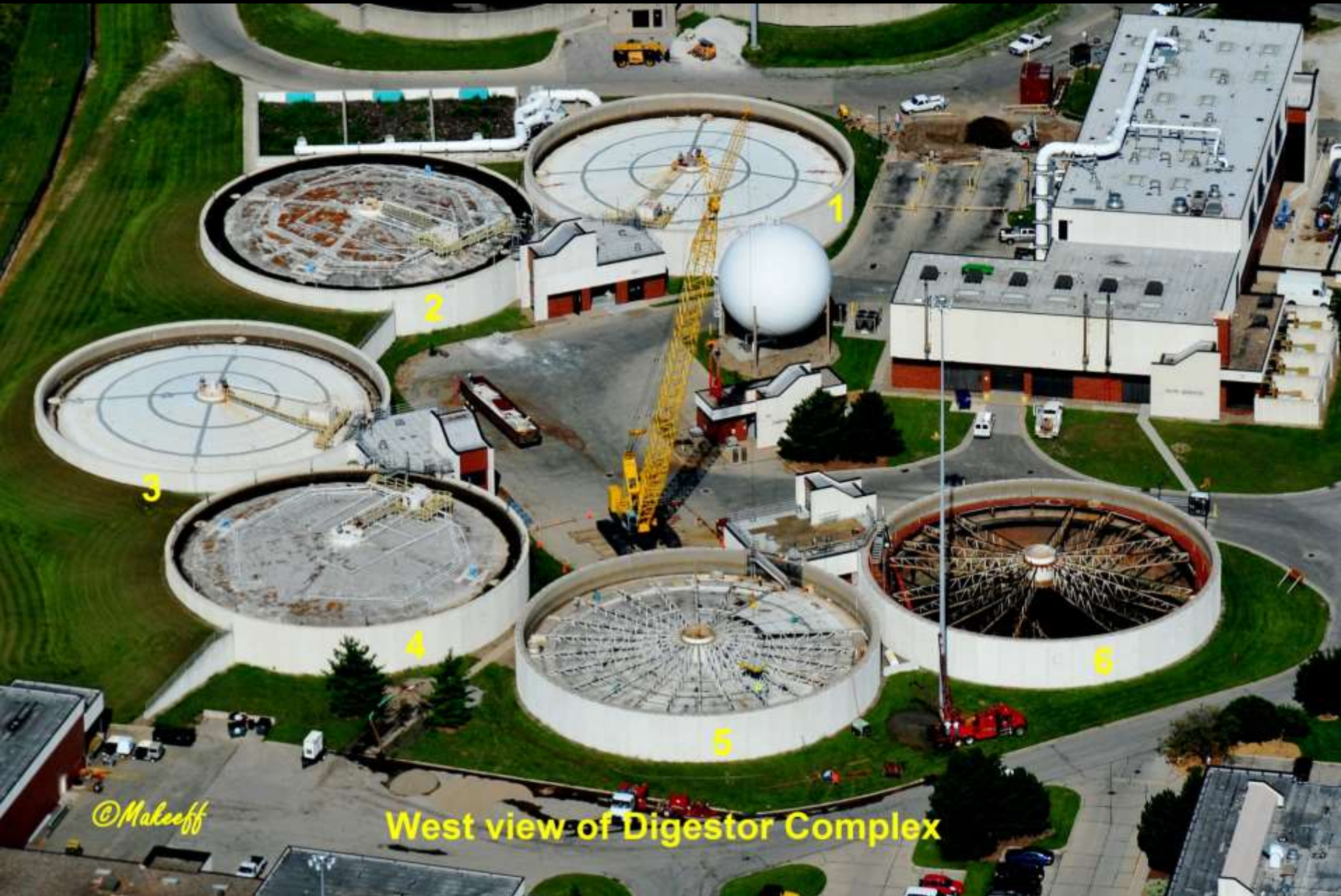


Below grade 170k gal.
Receiving Tank
~2007

A Wastewater and Hauled Organic Waste Treatment Center







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West view of Digester Complex





Biogas Production at Des Moines

- WRA is producing a significant amount of renewable fuel in digesters
- Capacity to increase biogas production with more hauled waste
- Changes in federal legislation are establishing renewable fuel standards, particularly for use in transportation fuels
- Environmental impacts of biogas
 - Biomethane production is carbon-neutral (does not add to greenhouse gas emissions)
 - Reduces consumption of natural gas, thus lowering CO₂ emissions
- Supports sustainability initiatives and goals of City of Des Moines and WRA

Project Organizational Chart





Development of Bioenergy Model

Financial Inputs		Process Information				
Electricity Cost, \$/kwh	\$0.0616	PSA 1500	PSA 2250	WS 1500	WS 2250	
Natural Gas Purchased, \$/MMBtu	\$6.86	% Recovery	95%	95%	98%	98%
Labor, \$/hr	\$60	Sales Gas %CH ₄	97%	97%	96.2%	96.2%
Water, \$/100 gal	\$0.40	Sales Gas HHV, BTU/cf	980	980	970	970
Lube Oil, \$/gal	\$15	Water, gpm	0	0	2.7	4.4
Polymer, \$/5 gal	\$700	Connected Load, hp	948	1294	842.9	1216.3
Air Emissions Fee, \$/ton	\$56	Natural Gas, MMBtu/day	48	72	0	0
Discount Factor	5%	Polymer, gal/yr	0	0	5	7.5
RIN Inflation, %/yr	5%	Compressor Heat Recovery, MMBtu/hr	0	0	0.0	0.0
Utilities Inflation, %/yr	5%	Tail Gas Heat Recovery, MMBtu/hr	3.4	5.1	0.0	0
Labor Inflation, %/yr	5%	Lube Oil, gpd	Included below		4	6.5
Maintenance Inflation, %/yr	5%	Preventative Maintenance, \$/yr	\$72,000	\$91,260	\$50,500	\$50,500
MidAmerican Tariff Inflation, %/yr	5%	Labor, hr/yr	0	0	0.0	0.0
Air Emissions Fee Inflation, %/yr	5%	Downtime, hr/yr	0	0	0	0

Raw Gas Data		Initial Investment				
Raw Gas, %CH ₄	65%	PSA 1500	PSA 2250	WS 1500	WS 2250	
Raw Gas, H2S ppmv	4000	Equipment Capital, \$	\$2,350,000	\$3,042,000	\$2,556,000	#####
Raw Gas Flow Growth, %	0%	Thermal Oxidizer, \$	\$497,000	\$643,351	\$350,055	\$477,696

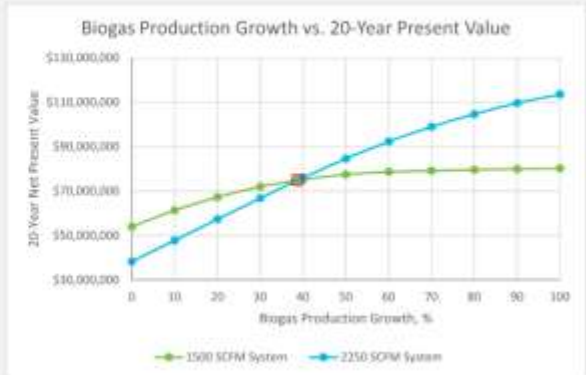
Sales Gas Economics	
Renewable Gas Sold, \$/MMBtu	\$5.00
Monthly Customer Charge, \$/month	\$1,315
Commodity Charge, \$/therm transported	\$0.00495
Demand Charge, \$/MDR therms/month	\$0.52886

Environmental Attributes	
RIN Value, \$/RIN	\$0.65
RIN Conversion, RIN/MMBtu	11.727
RIN Value, \$/MMBtu	\$7.62

Percent of Gas Accepted	
1500 SCFM System	99.1%
2250 SCFM System	100.0%



20-Year Economics, Present Value				
	PSA 1500	PSA 2250	WS 1500	WS 2250
Capital	\$9,855,000	\$11,921,000	\$9,475,000	\$12,086,000
Total Annual Costs	\$36,304,000	\$52,772,000	\$33,288,000	\$36,665,000
Total Annual Revenue	\$100,162,000	\$103,050,000	\$98,914,000	\$99,784,000
20 Year Overall Revenue	\$54,003,000	\$38,357,000	\$56,151,000	\$51,033,000
Payback Period, months	37	57	35	46



Design Criteria

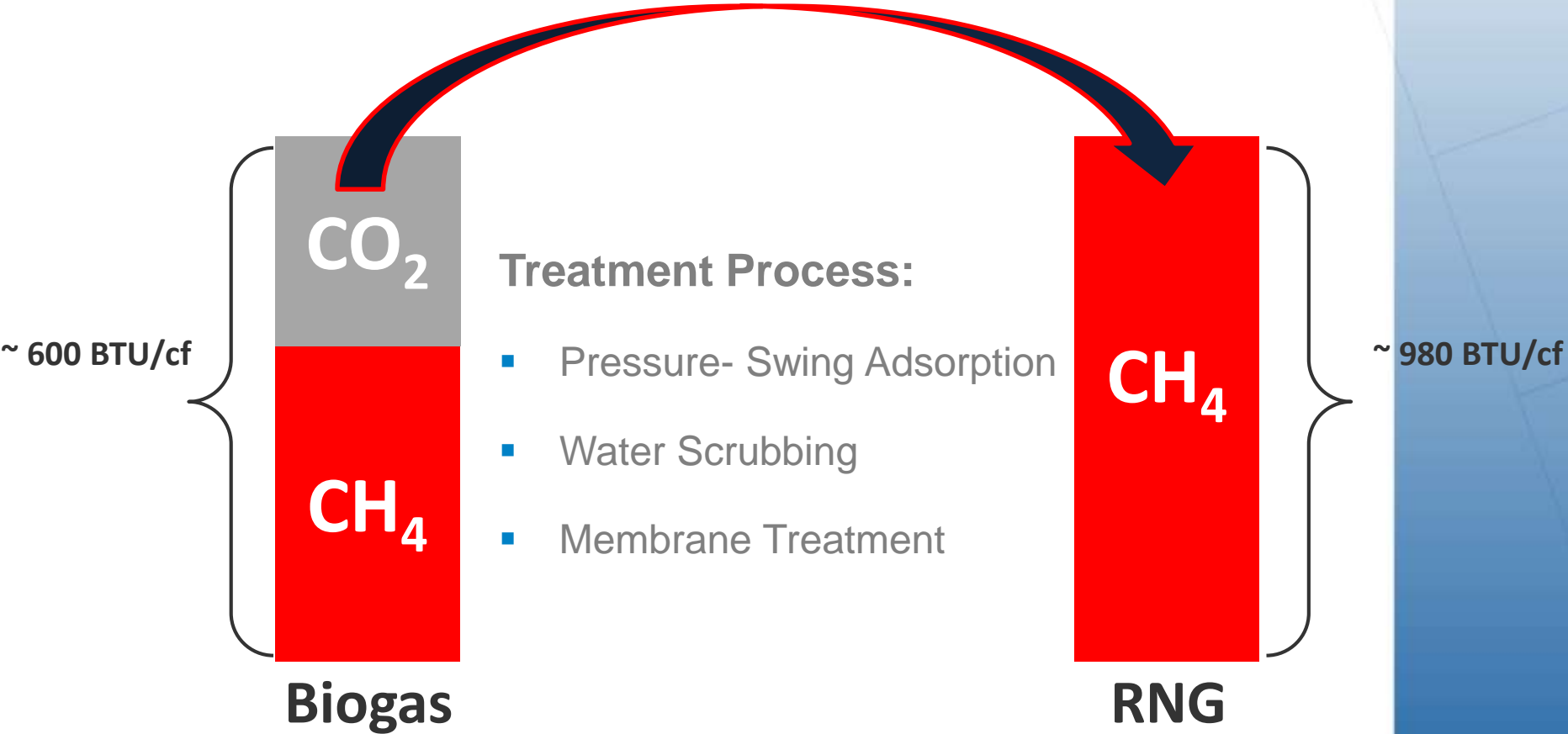


- Inlet Biogas Flow: 2250 SCFM

Component	Digester Gas	Pipeline Specification
BTU Content	~660 BTU/scf	> 950 BTU/scf
Carbon dioxide	35%	< 3% by volume
Nitrogen	0.7%	< 4% by volume
Total Inerts (N ₂ + CO ₂)	~36%	< 5% by volume
Oxygen	<0.2%	< 0.3% by volume
Water	Saturated	< 5 lb/mmscf
Hydrogen sulfide	Actual: 50-600 ppm Design: 6,000 ppm	< 0.25 grain/Ccf
Total Sulfur	N/A	< 20 grain/Ccf
Volatile Organic Compounds	10-30 ppm	0 ppm

Technology Comparison

Biogas → Renewable Natural Gas (RNG)



Membrane Scrubbing System

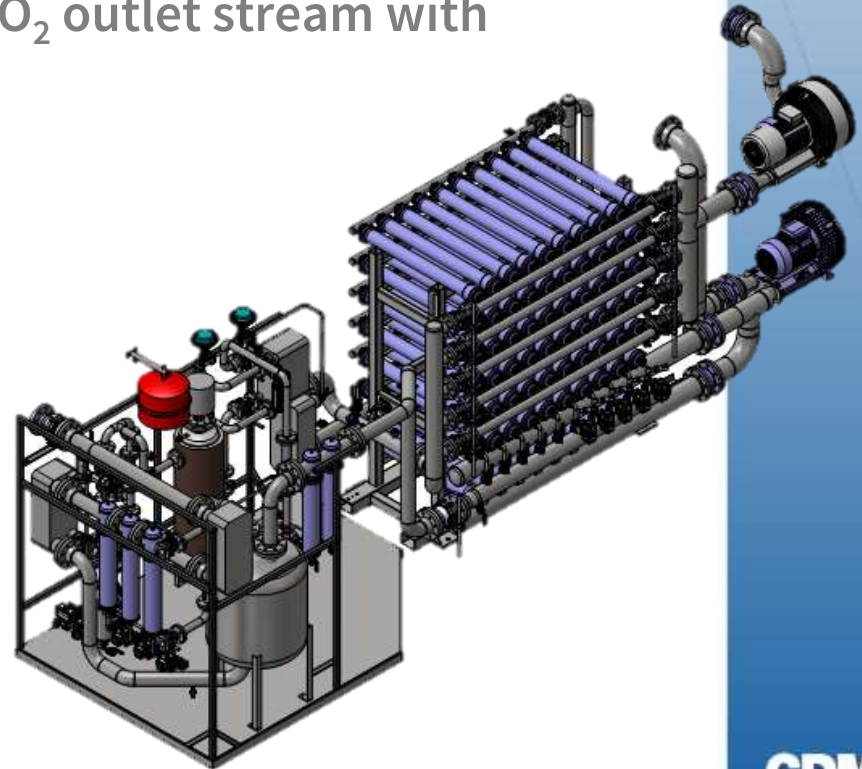


- System Description

- Utilizes physical diffusion process through membranes which use a thin polymer film. Membrane selectively retains CH_4 and some N_2 (~20%) and O_2 (~50%)
- Generates very high quality CO_2 outlet stream with approximately 1-2% CH_4

- Typical Components

- Compressor
- Gas Heat Exchanger
- H_2S Scrubbing System
- Siloxane Carbon Filters
- Chiller
- Final Polishing Filters
- Membranes





Membrane Scrubbing System

- **Manufacturers**
 - DMT Environmental Solutions (Joure, Netherlands)
 - Unison Solutions (Dubuque, Iowa)
 - Greenlane (New Zealand, USA)

- **Advantages**
 - Removes some O₂ (~50%) and N₂ (~20%)
 - High CH₄ recovery (97-99.5%)
 - *Depending on the number of stages*
 - High level of turndown (~10%)
 - Dry process

- **Disadvantages**
 - No U.S. Installations
 - H₂S and siloxane pretreatment required
 - Limited data on membrane life and fouling

Liquid Scrubber System

- System Description
 - Separation by physical adsorption in scrubber
 - Water is transfer solvent; performance follows Henry's Law- CO_2 is more soluble in water than CH_4
 - Upflow packed towers with polypropylene media
 - Solvent regenerates in stripping tower and only small daily make-up water demand

- Typical Components
 - Compressor
 - Scrubber Vessel
 - Flashing Vessel
 - Stripping Vessel
 - Compressor Radiator Skid
 - PSA/TSA Adsorber (gas drier)
 - Process Water Chiller





Liquid Scrubber System

- **Manufacturers**
 - Greenlane (New Zealand, USA)
 - DMT (Netherlands, USA)
 - Malmberg (Sweden)

- **Advantages**
 - Proven technology – multiple installations globally and in USA
 - Non-toxic solvent (water)
 - Also removes H_2S in inlet biogas
 - Moderate CH_4 losses (~2% slip)

- **Disadvantages**
 - Increases H_2O , O_2 , and N_2
 - Tail gas treatment is required
 - Very tall outdoor vessels

Pressure Swing Adsorption (PSA)

- System Description
 - Biogas is pressurized to flow up through the adsorption vessels
 - Contaminants are trapped by media designed to not capture CH₄
 - Vacuum is applied to depressurize (i.e.; pressure swing) after adsorption to purge contaminants from vessel in tail gas stream
 - Process is batch but use of multiple vessels and rotary valve allow continuous flow

- Typical Components
 - Compressor
 - Water Separator
 - Air Fan Cooler
 - Adsorber Vessels and Valve Skid
 - Vacuum Pumps
 - Buffer Tanks



Zeolite Media



Pressure Swing Adsorption

- **Manufacturers**
 - Guild Associates Inc. (Dublin, Ohio)
 - Xebec Adsorption Inc. (Quebec, Canada)

- **Advantages**
 - No H₂S pretreatment required for <6,000 ppm (Guild only)
 - Simple, one step, dry process that is proven technology
 - Media is regenerative
 - Spare parts are generic. Can be serviced by plant operators or local mechanic

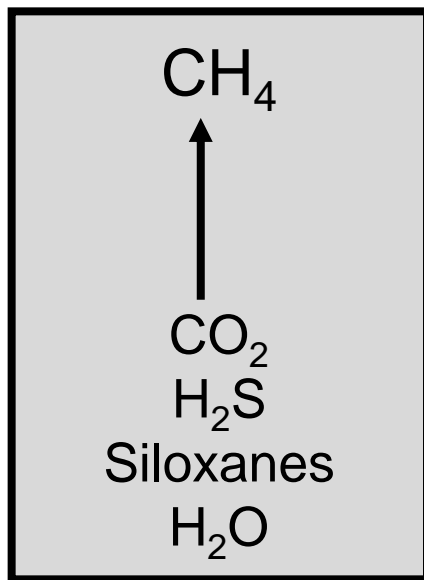
- **Disadvantages**
 - Methane recovery is lower (95%)
 - Additional PSA vessels required for O₂/N₂ removal if air is in the biogas
 - Tail gas treatment is required

PSA Flow Schematic



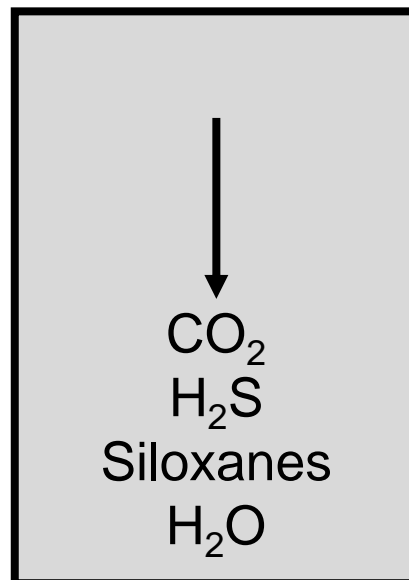
Adsorption
Cycle

Purified Gas



Biogas

Small Methane
Purge



Vacuum
Pump

Tail Gas
to TO

Regen
Cycle

PSA Batch Cycles



ADSORPTION	DEPRESSURIZE	VACUUM & PURGE	REPRESSURIZE
REPRESSURIZE	ADSORPTION	DEPRESSURIZE	VACUUM & PURGE
VACUUM & PURGE	REPRESSURIZE	ADSORPTION	DEPRESSURIZE
DEPRESSURIZE	VACUUM & PURGE	REPRESSURIZE	ADSORPTION

Technology Comparison & Selection



- Hydrogen Sulfide Considerations
 - Membranes: pre-treatment required
 - Water Scrubber: maximum inlet ~2,500 ppm H₂S
 - *Tail gas treatment required (biofilter or RTO)*
 - PSA: maximum inlet ~ 6,000 ppm H₂S
 - *Tail gas treatment required (TO)*

- System Recovery Performance
 - Membranes: high methane recovery
 - Water scrubber: high methane recovery, increases oxygen
 - PSA: lower methane recovery

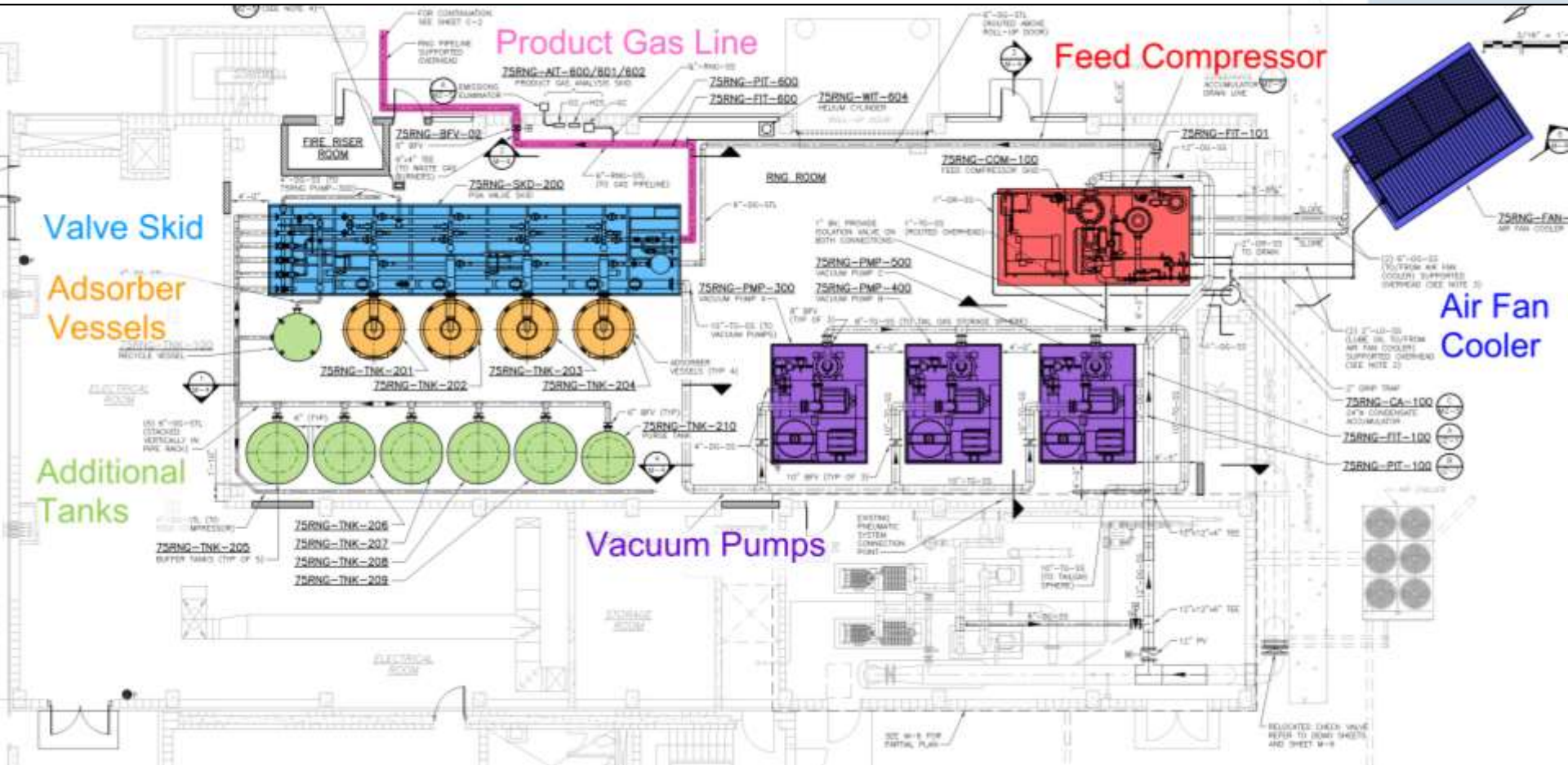
- Technology Selection:
 - PSA System
 - Capacity of 2,250 scfm inlet biogas flows
 - Thermal Oxidizer with heat recovery

Project Design

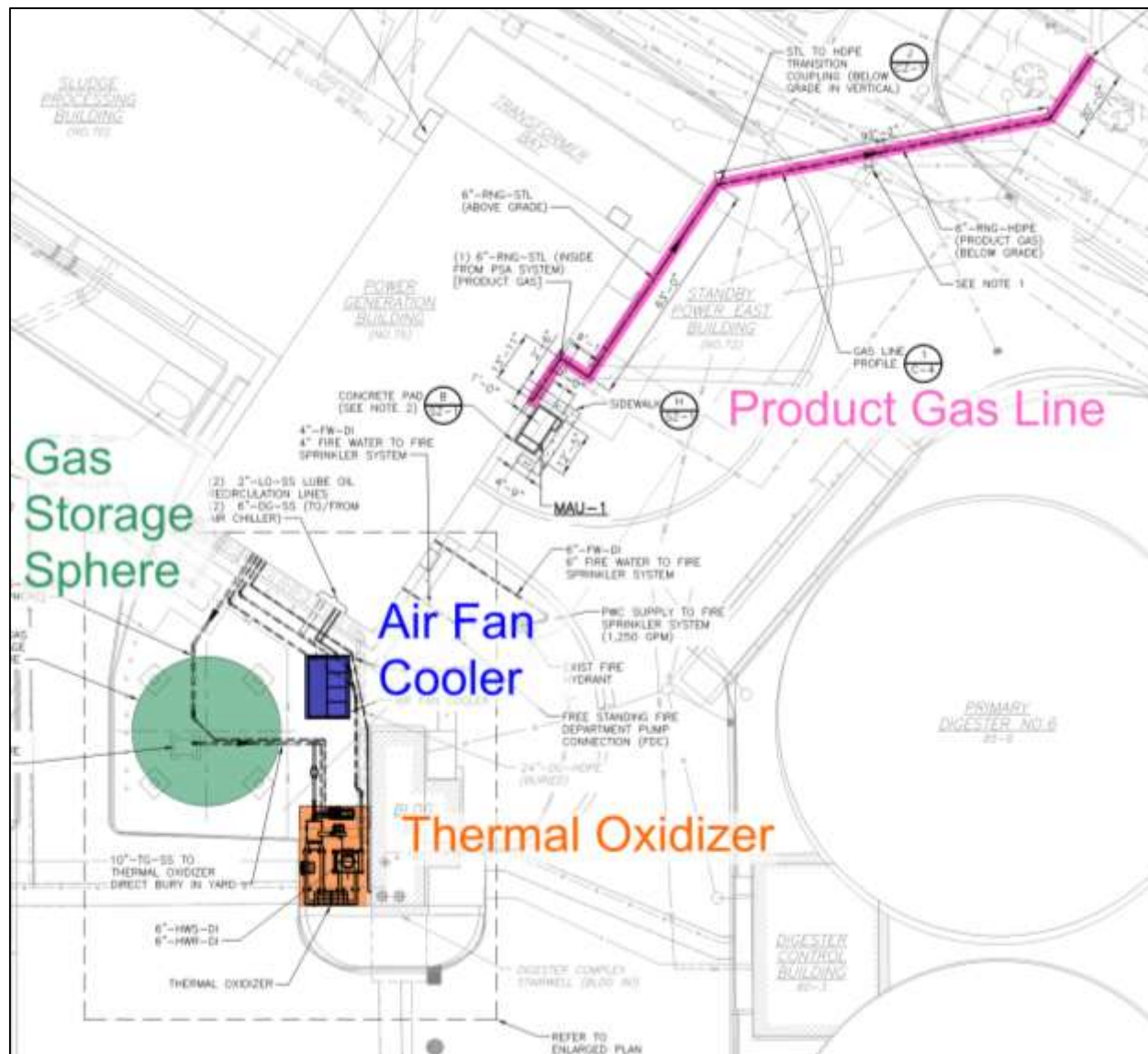




System Layout



Site Plan



Area Classification & Building Modifications

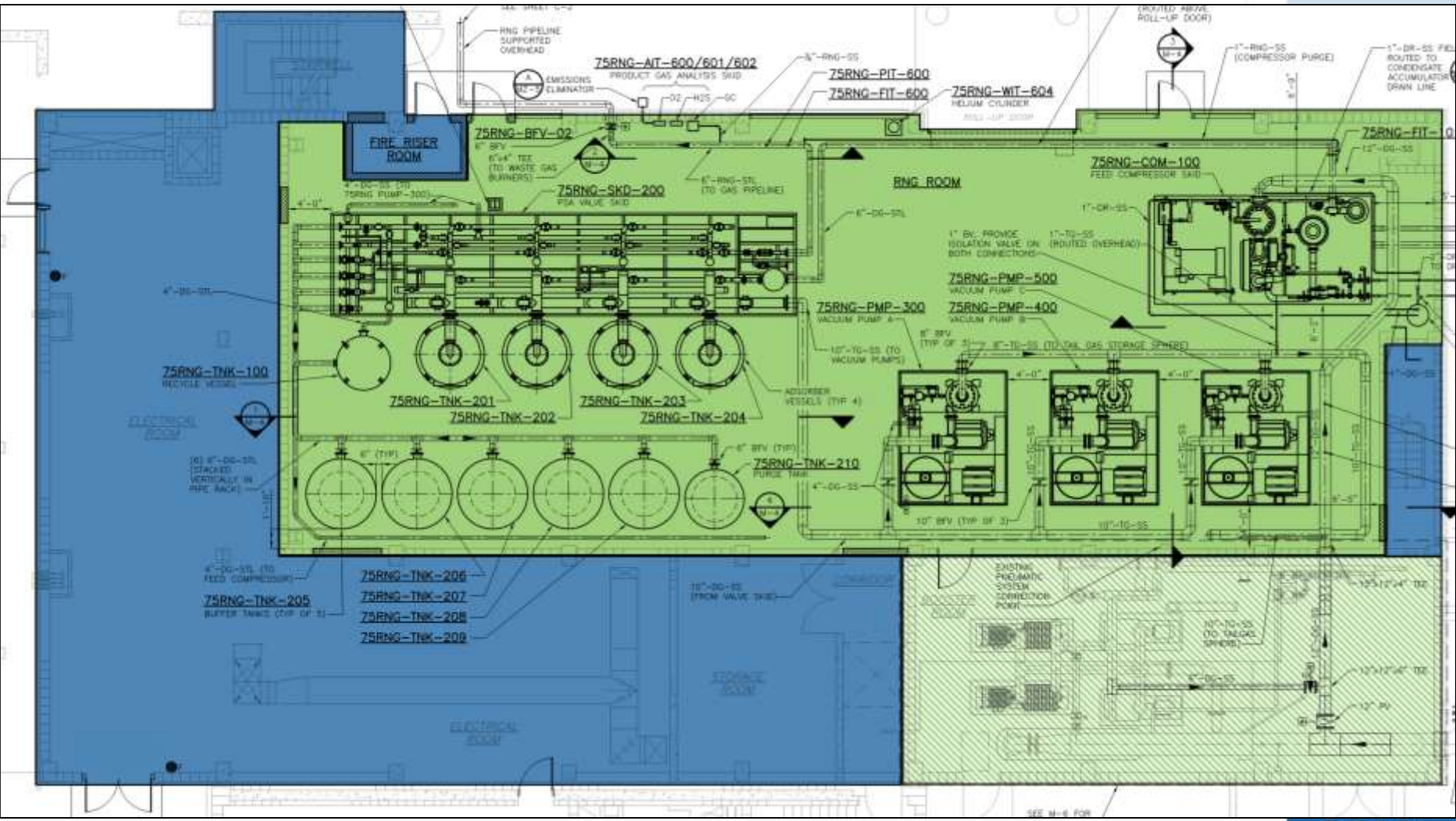


- NFPA defines requirements of “Digester Gas Processing Rooms” involving biogas compression, handling, and processing equipment

Row	Location and Function	Ventilation Rate	Extent of Classified Area	NEC Area Electrical Classification	Material of Construction & Fire Protection Measures (2)
Row 18a	DIGESTER GAS PROCESSING ROOMS (Gas compression,	No ventilation or ventilated at less than 12 air changes per hours	Entire room	Class 1, Division 1, Group D	NC, CGD, H, FE
Row 18b	handling, and processing)	Continuously ventilated at 12 air changes per hour	Within 1.5m (5-ft) of equipment	Class 1, Division 1, Group D	NC, LC, CGD, H, FE
Row 18c		Continuously ventilated at 12 air changes per hour	Entire Room	Class 1, Division 2, Group D	NC, LC, CGD, H, FE

NC – Noncombustible Material; LC – Limited-combustible material; CGD – Combustible Gas Detection System; H – Hydrant Protection; FE – Portable Fire Extinguisher

Area Classification Plan



Current Project Status

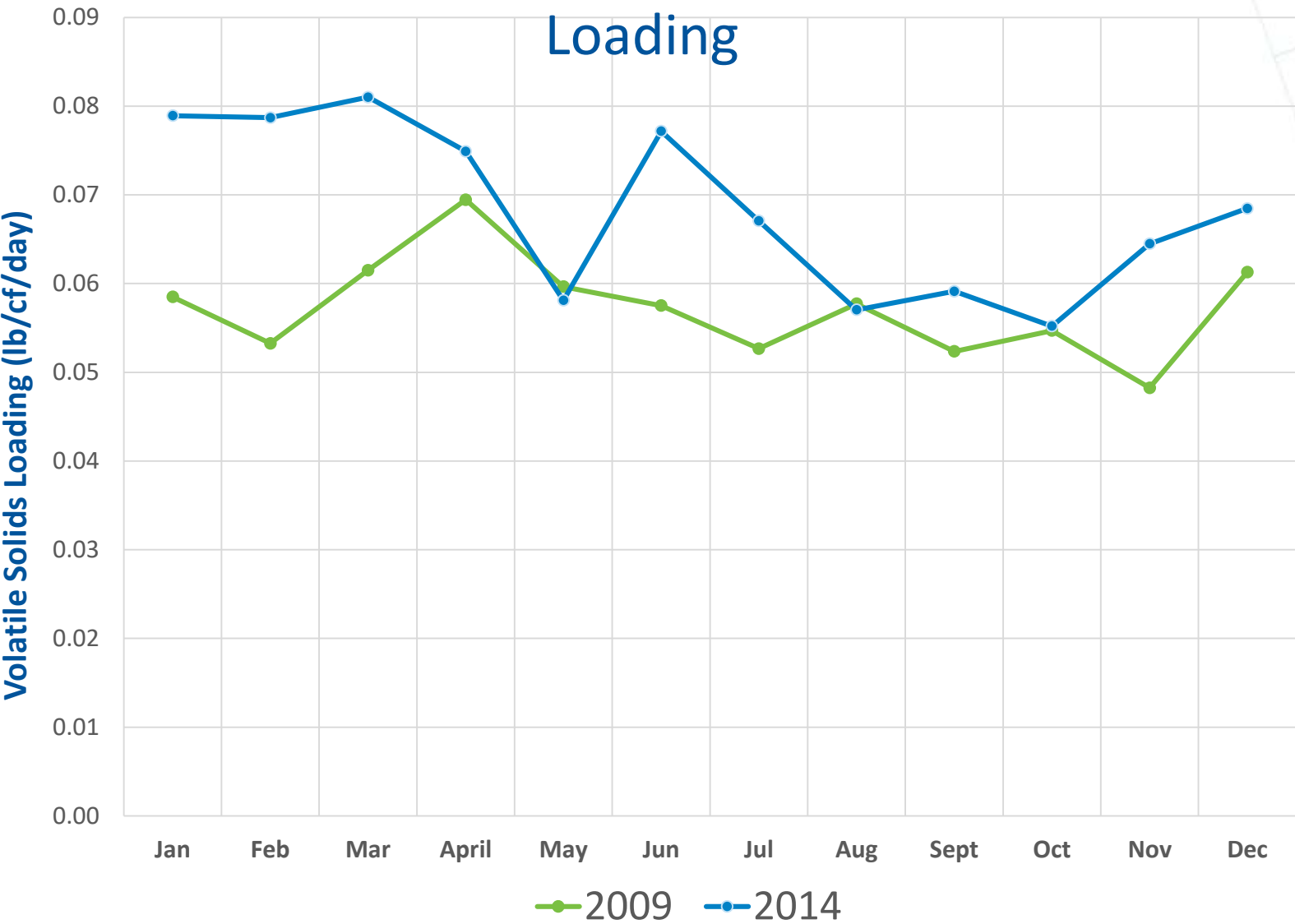


- 100%: October 2016
- Construction duration: approximately 1 year
- Construction Capital Costs ~\$12M
- Project Payback of ~4yrs
- Current value of RNG Injection + RIN credits is \$10k a DAY!



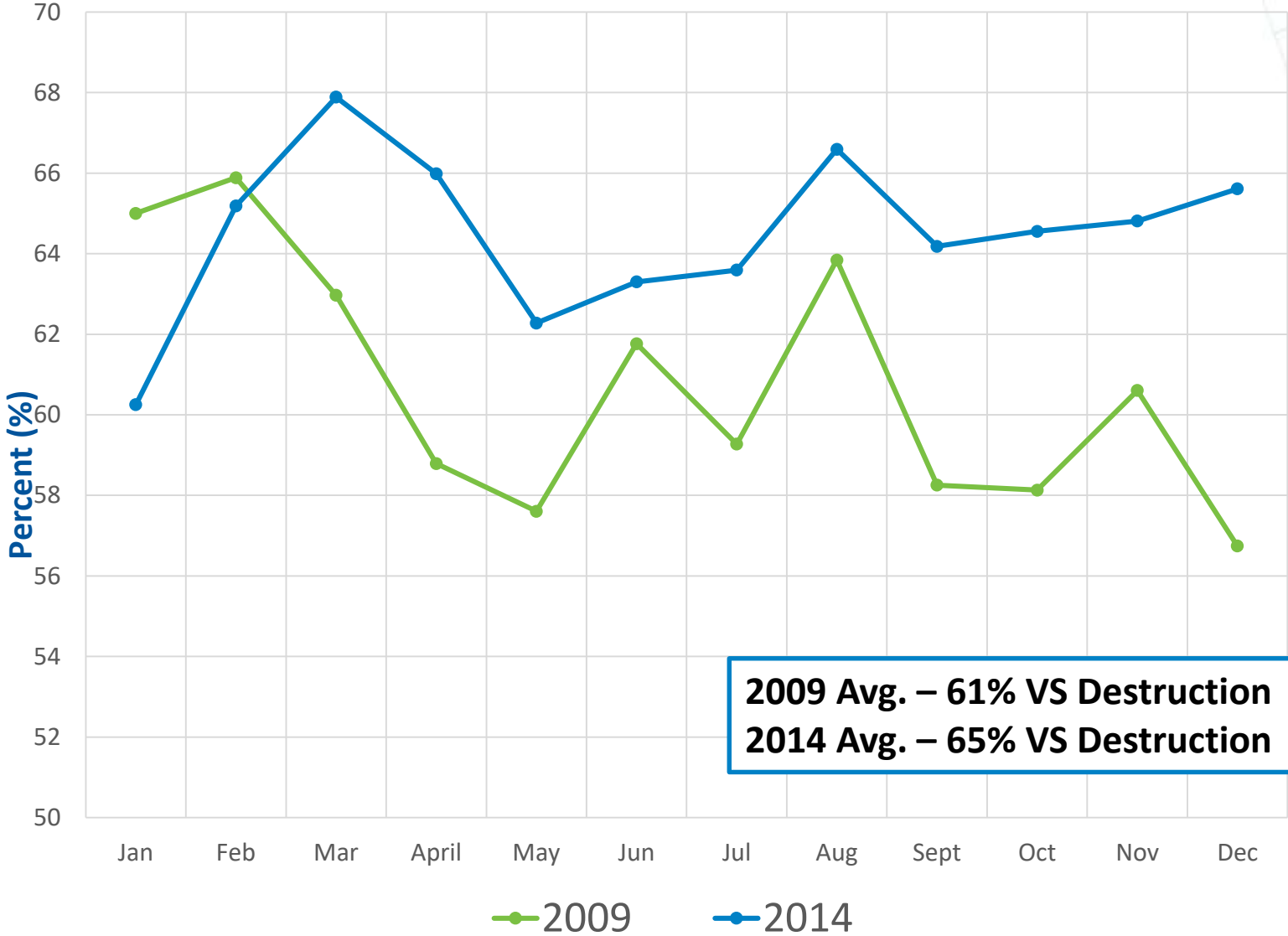
Blended Sludge Feed – Volatile Solids

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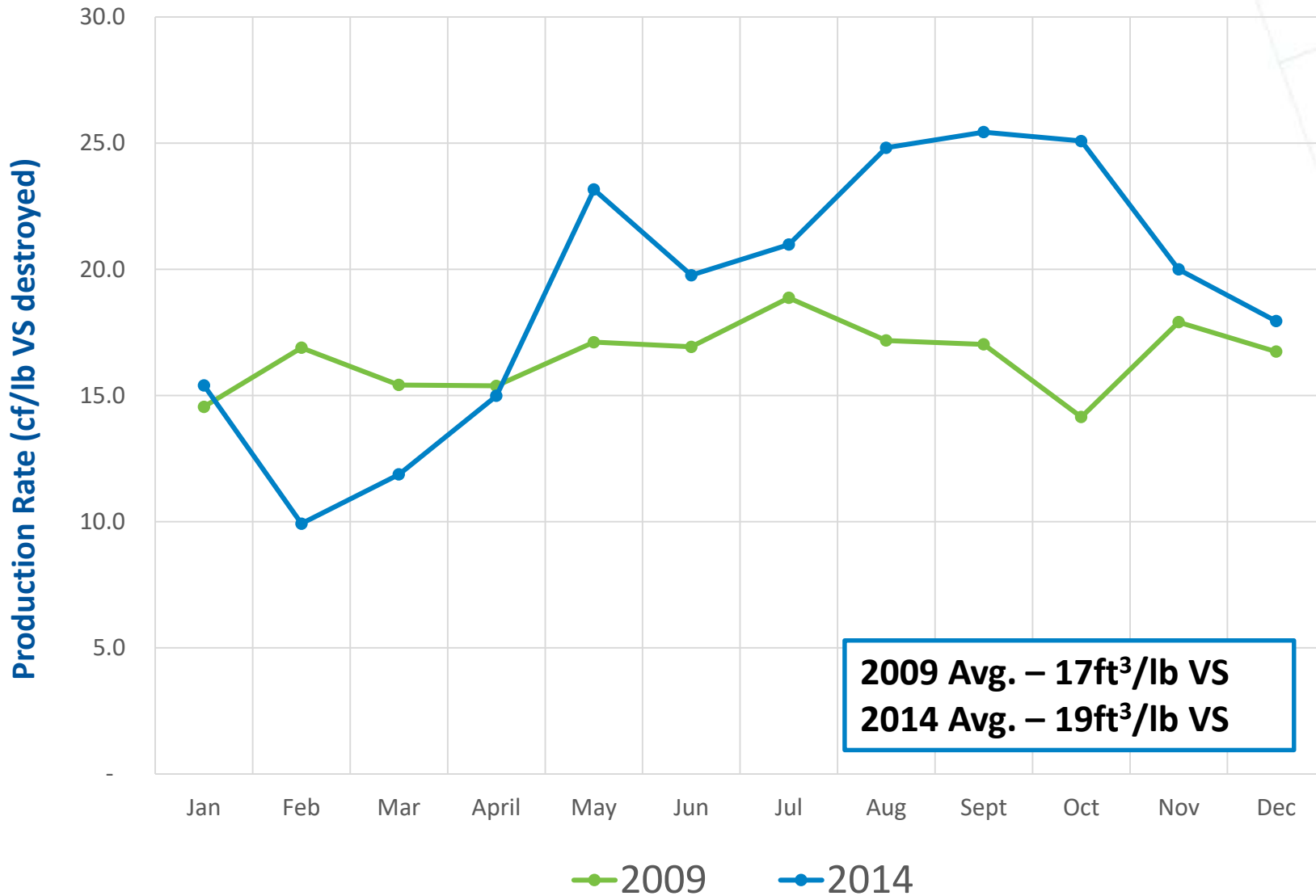




Volatile Solids Reduction

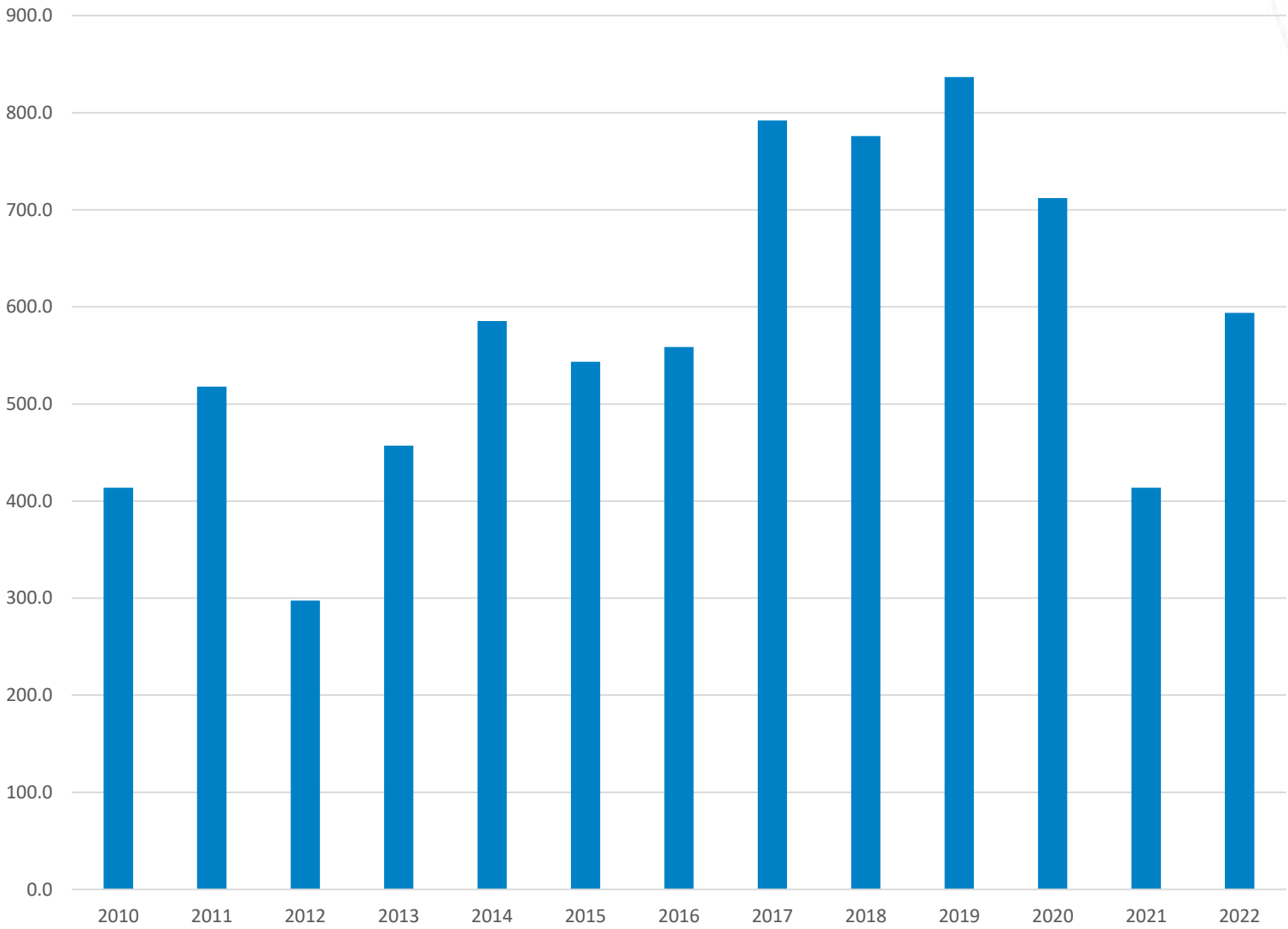


Average Biogas Production Rate



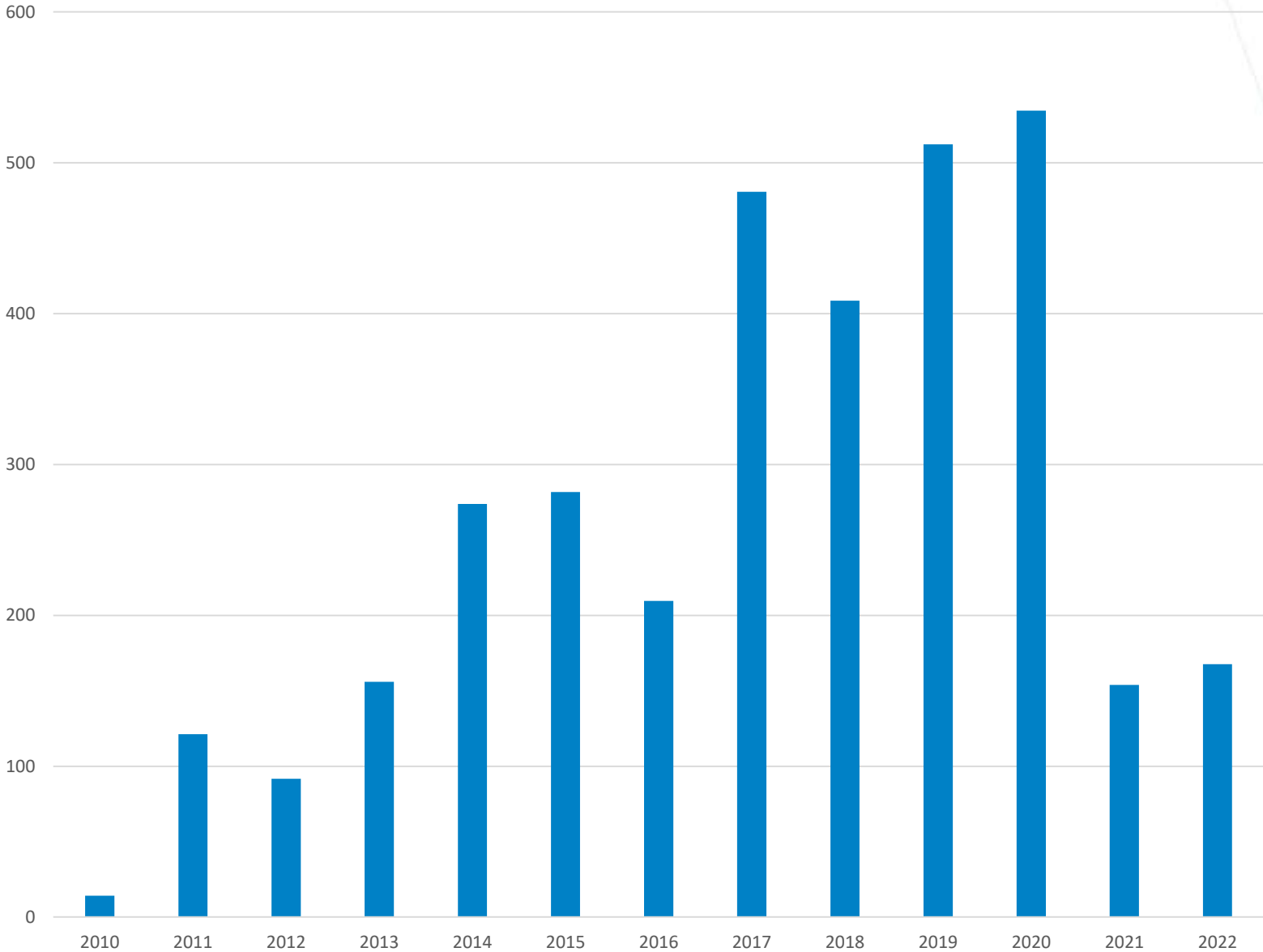


Total Biogas Produced (Million Cubic Feet)



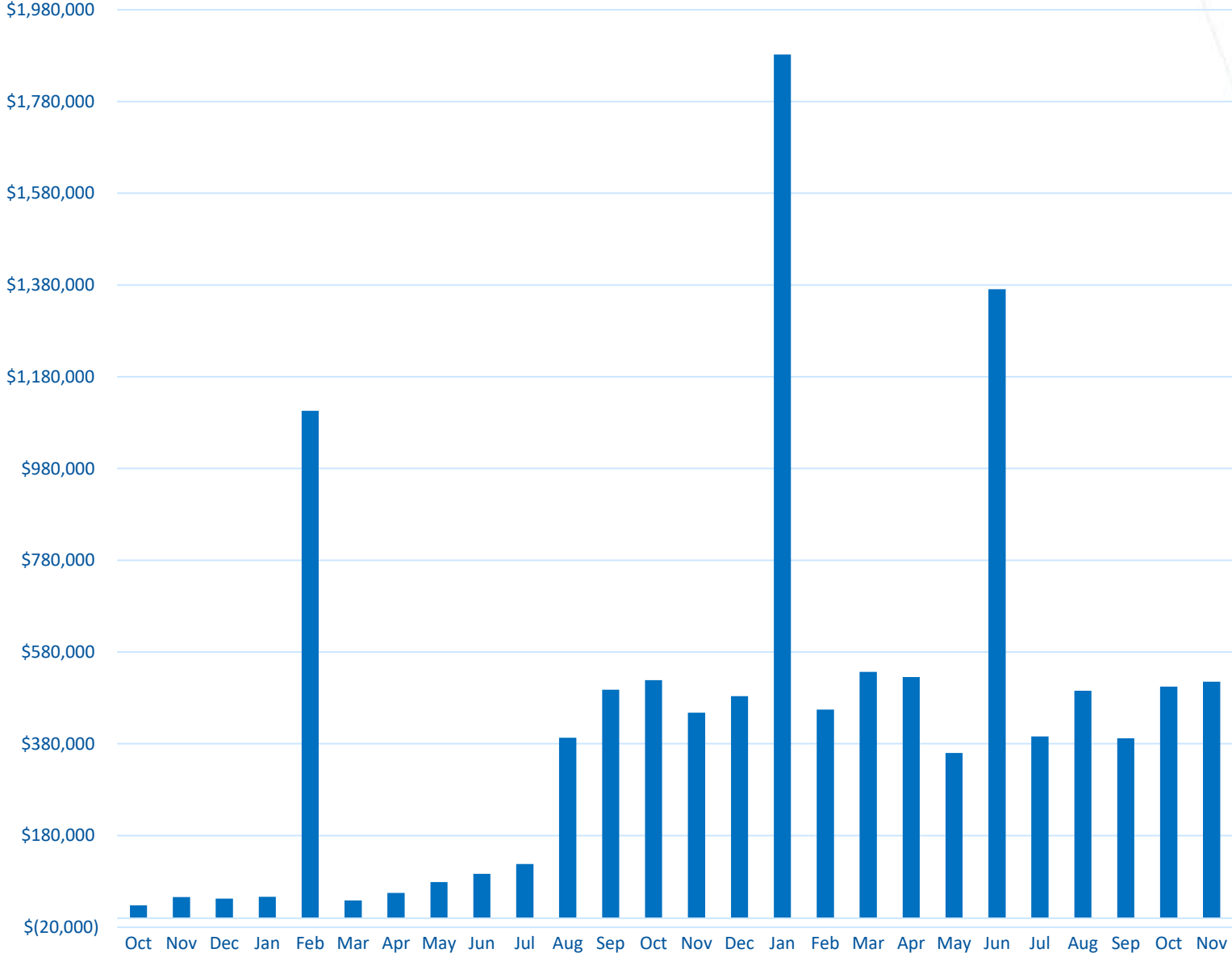


Total Biogas Wasted (Million Cubic Feet)





Renewable Natural Gas - Net Revenue Earned



Bio Gas - RNG Process 2021/2022/2023

